

- Process of treating
- Results from operation
- Operational problems

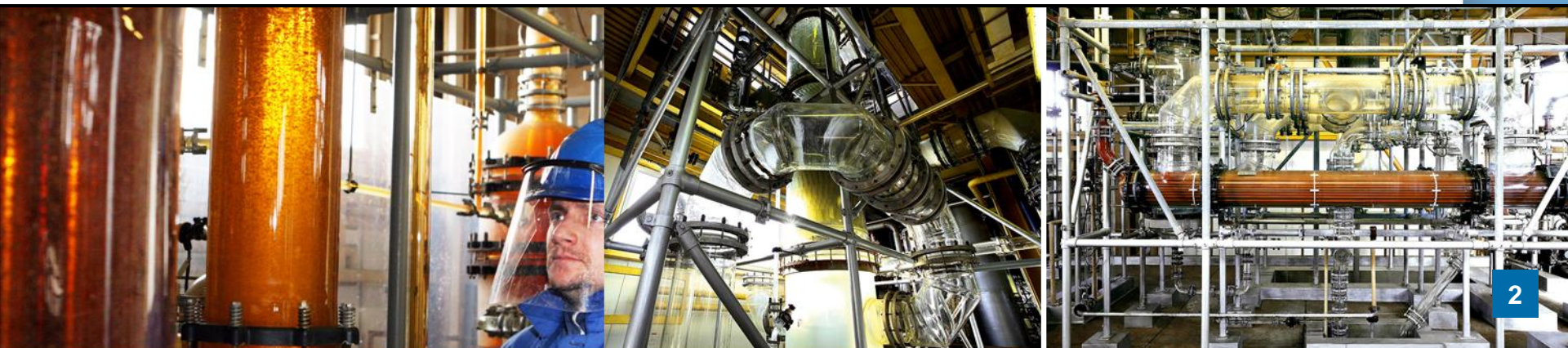
Radim Staněk

Treatment of wastewater from nitrocellulose production

Quality and Amount of Wastewater

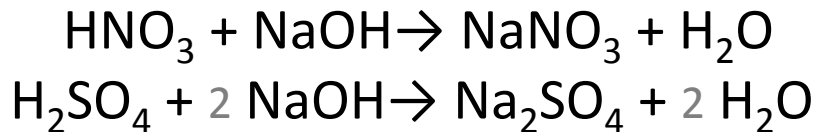
mg/L	pH	N-NO ₃ ⁻	SO ₄ ²⁻	COD	TSS
Wastewater	1 - 2	100 - 400	1,000 – 2,000	50 - 100	0 - 30

- Volume of wastewater is about 2,000,000 m³/year
- Temperature from 15 °C to 35°C
- It is necessary to adjust pH and remove nitrates

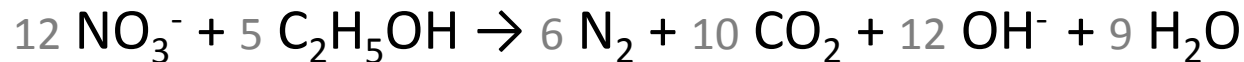


Princip of treatment

Neutralization by sodium hydroxide



Denitrification - bacteria use nitrate as electron-acceptor in the respiration chain instead of oxygen under anaerobic conditions:

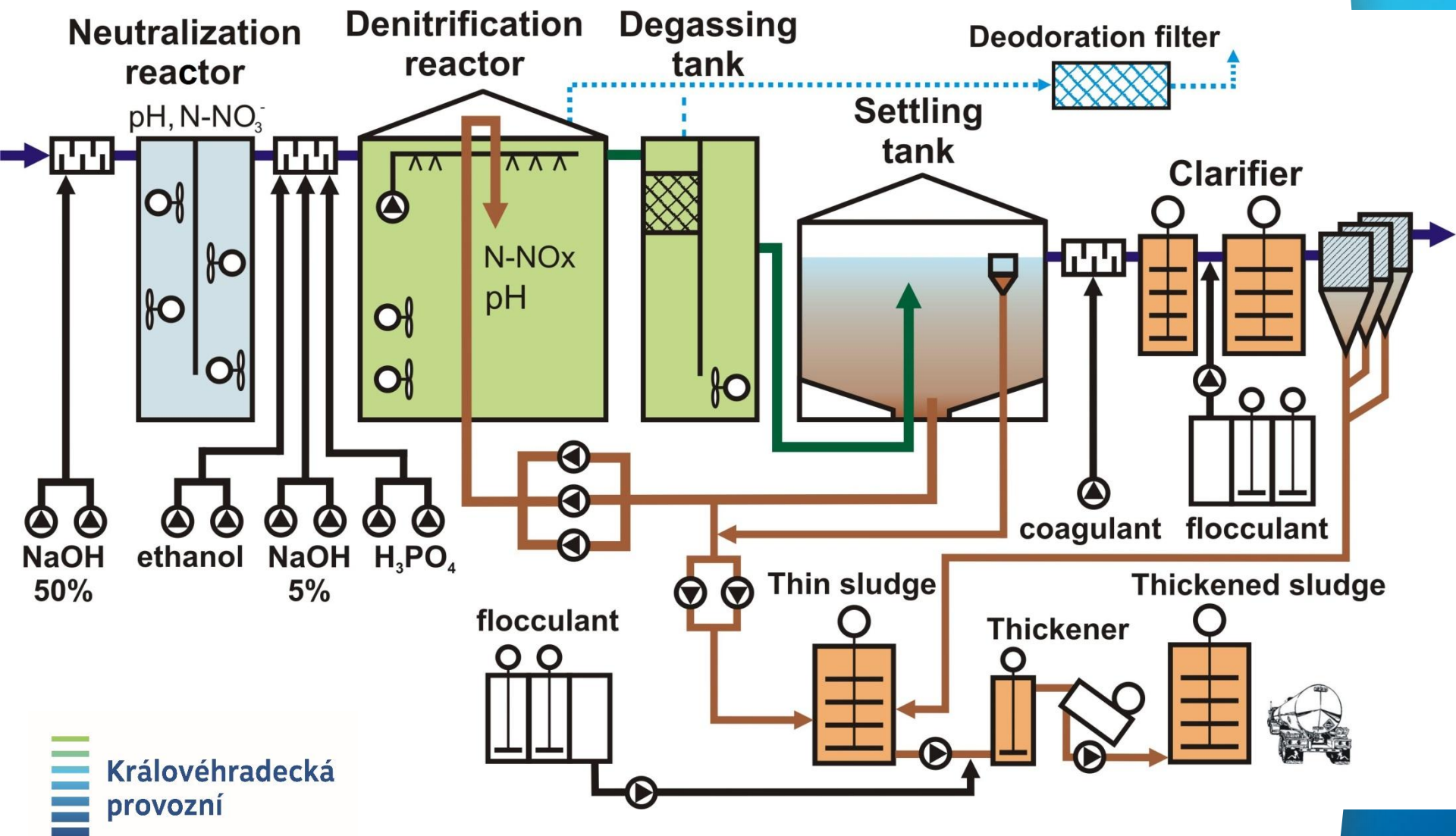


- 2.86 g COD are needed per gram of nitrate-nitrogen
- pH is increasing because hydroxide ions are produced

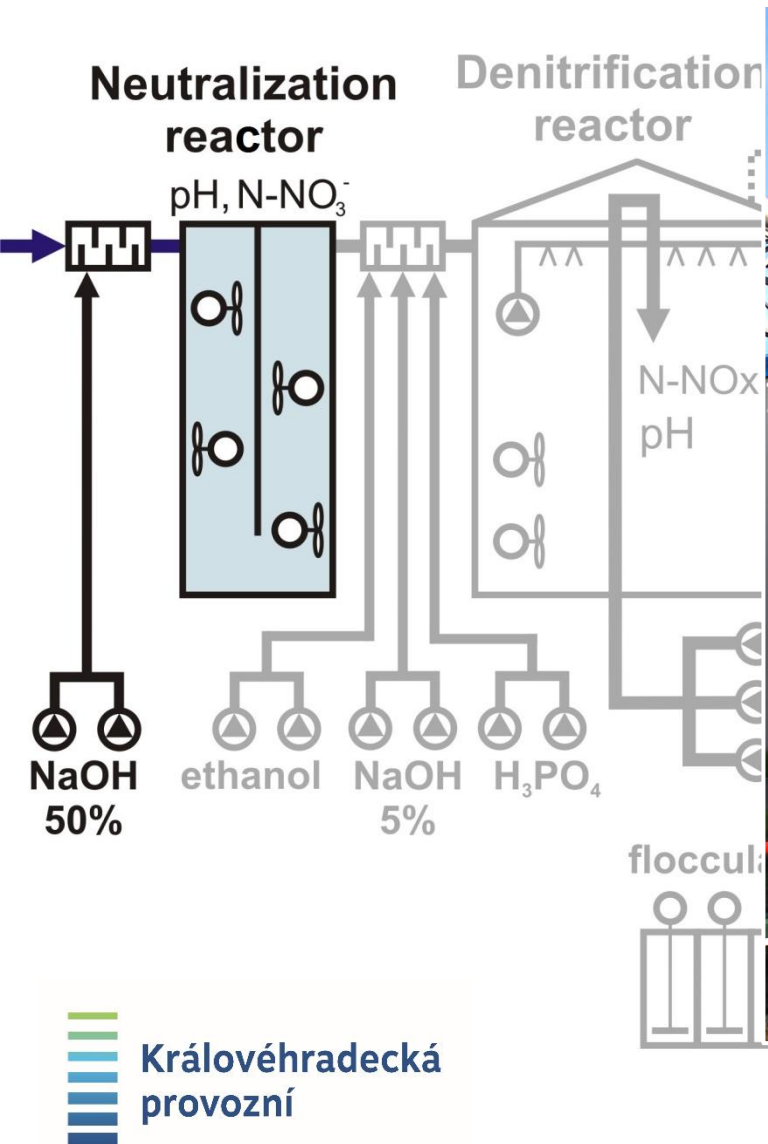
Complete denitrification pathway:



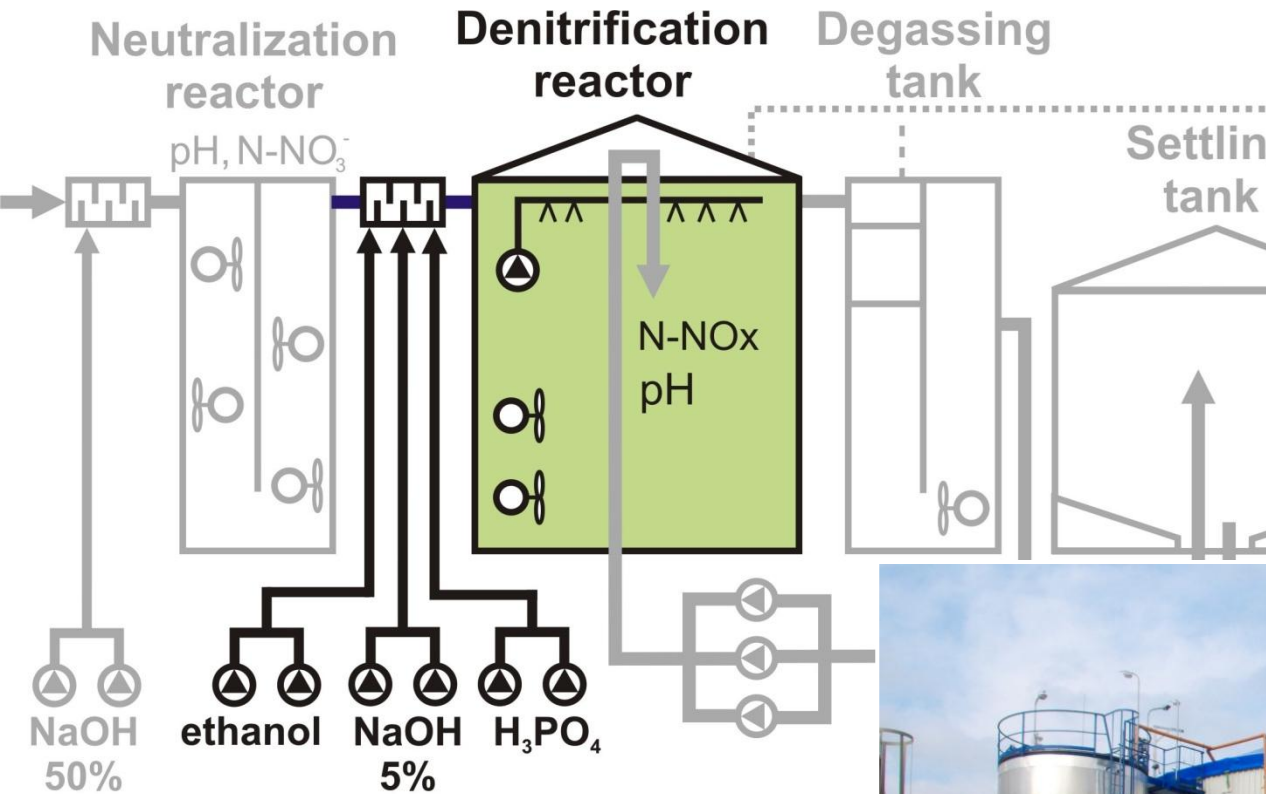
Process flow scheme



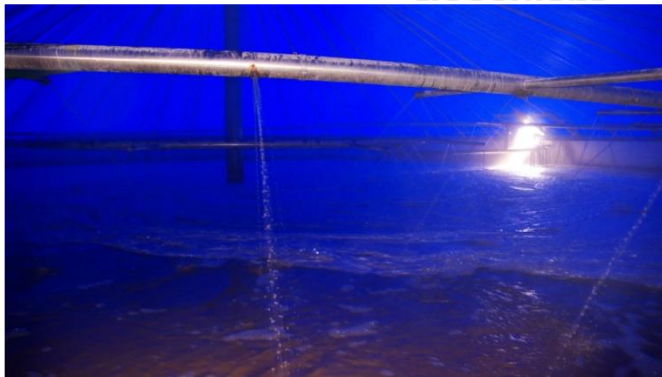
Neutralization



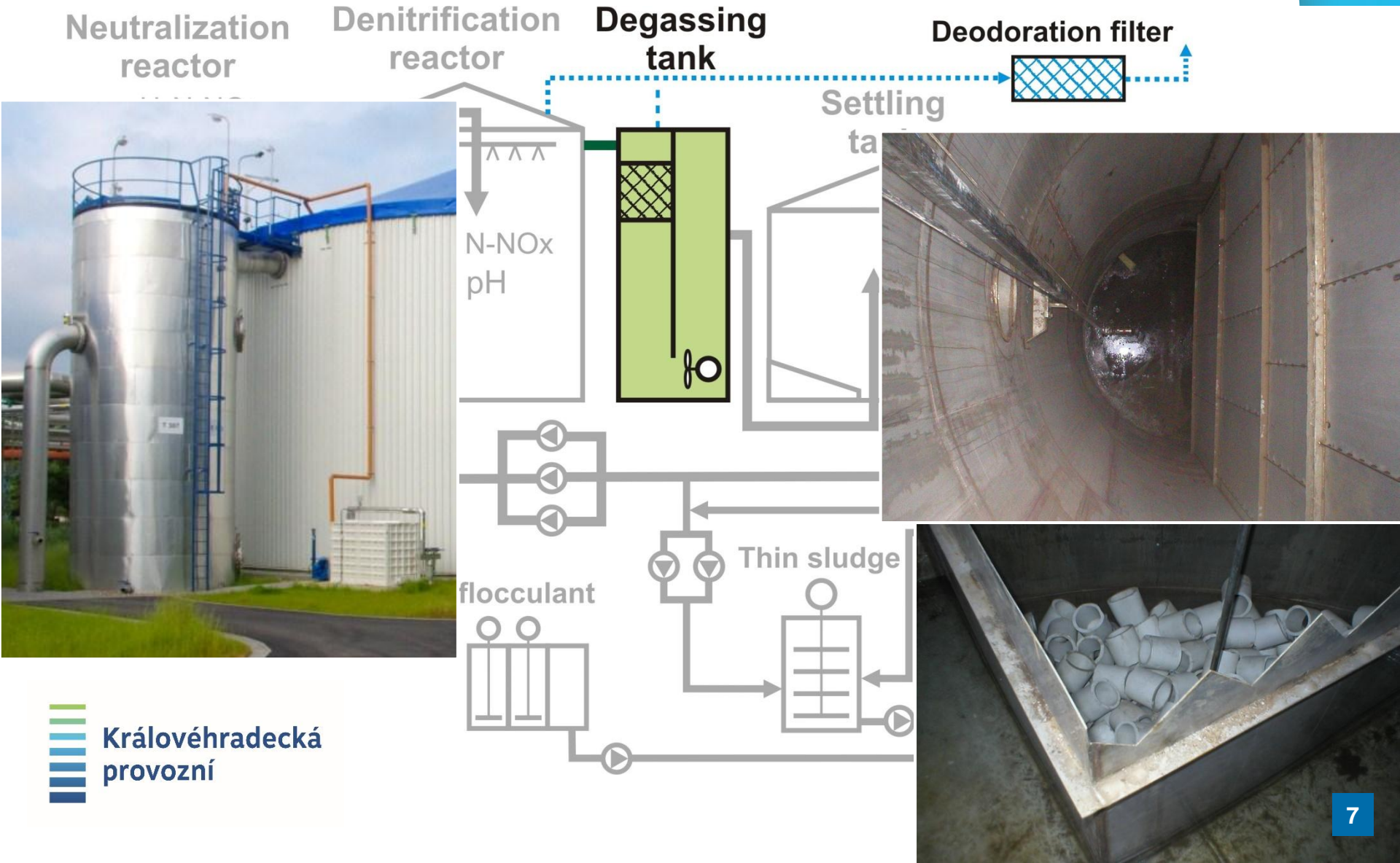
Denitrification



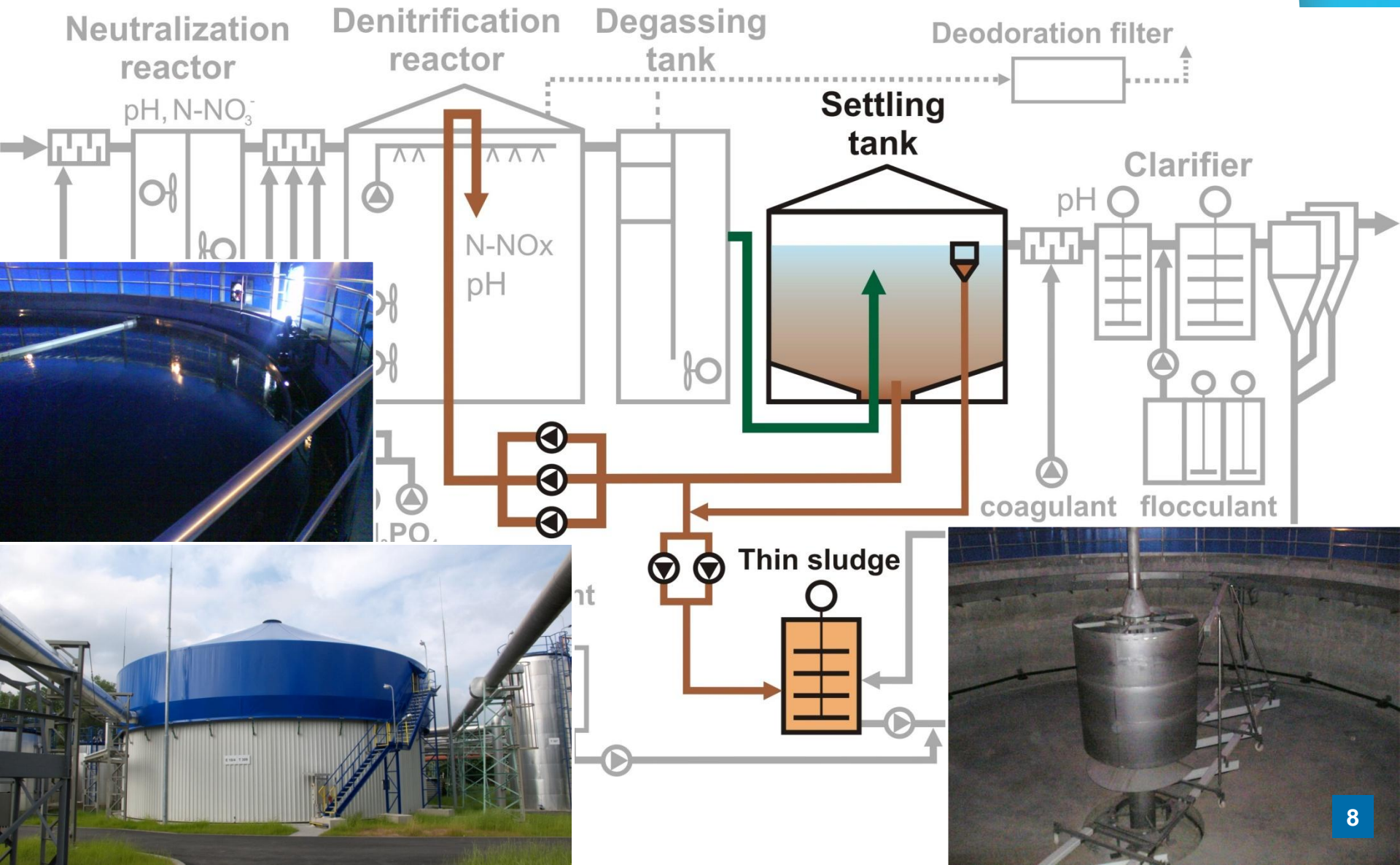
Deodorization filter



Degassing

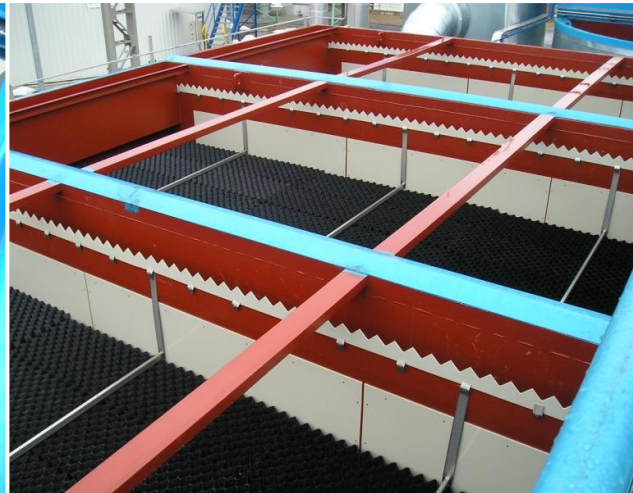


Separation of Sludge



Tertiary Treatment

Neutralization Denitrification Degassing

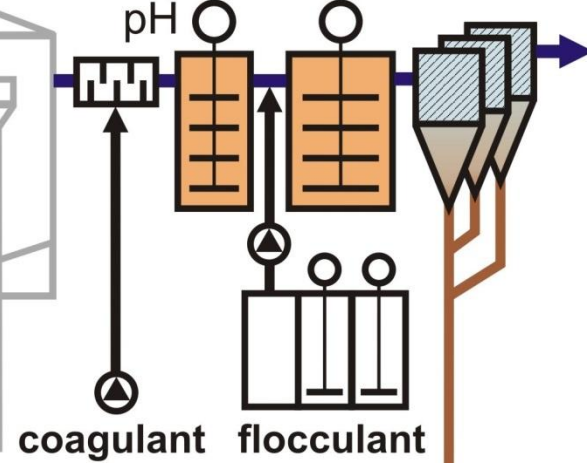


Deodorization filter



Clarifier

pH



coagulant

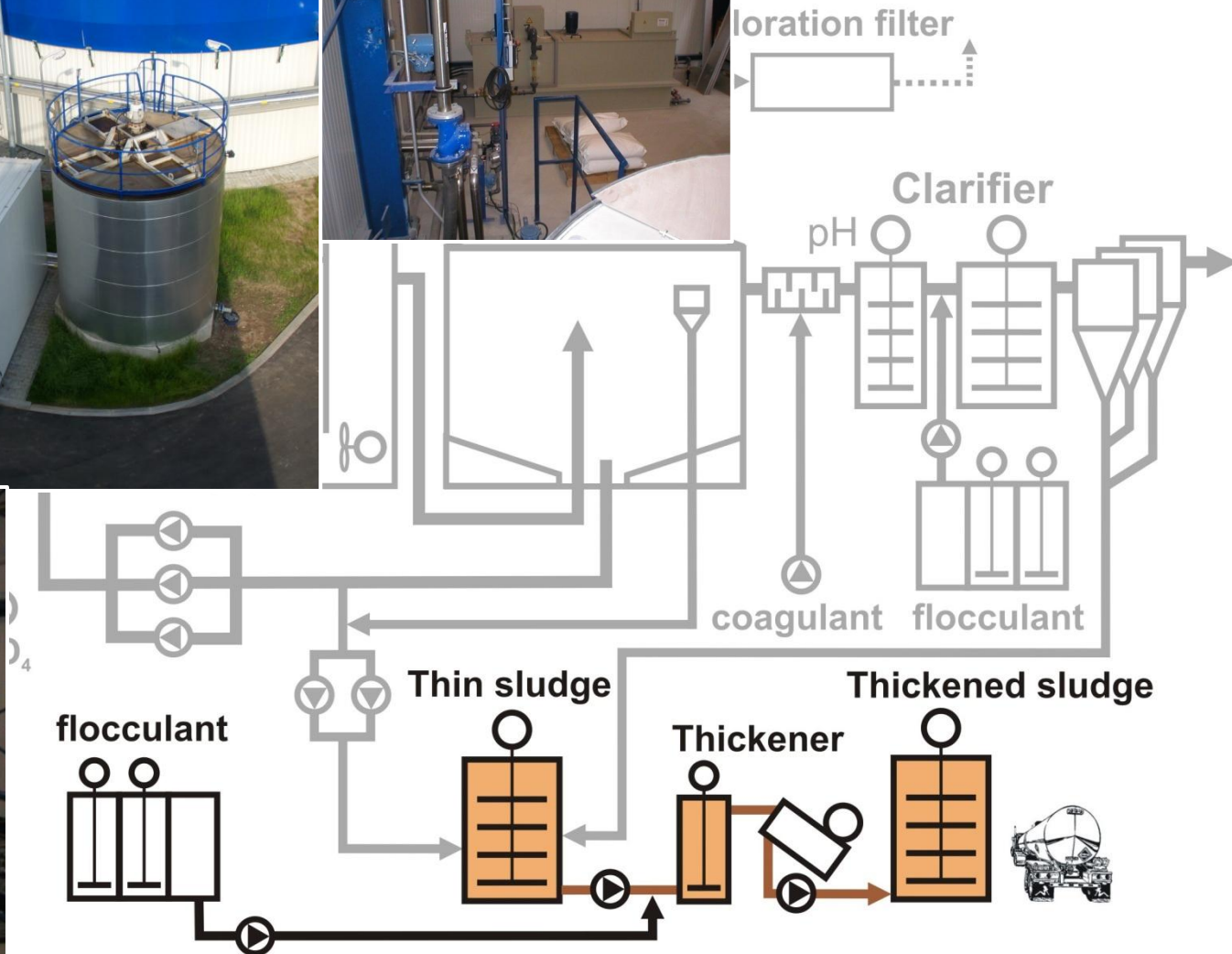
flocculant

Thin sludge

Thickened sludge

Thickener

Sludge Management



Hydraulic and mass loading

Volume of wastewater	
5200 m ³ /d	60 L/s (40 – 100 L/s)

Acidity	NaOH			ratio
kmol/d	m ³ 50%/d	t 100%/d	kmol/d	mol NaOH/mol acidity
176	8,0	6,0	150	0,80

20% of acidity is neutralized by hydroxide ions produced in denitrification.

$\Delta \text{N-NO}_3^-$	ethanol	Total consumed COD		ratio
t/d	m ³ /d	t/d	PE	t COD/t N
1.1	2.4	3.8	32,000	3.6

Technological Parameters

Sludge concentration (MLSS)	2 - 3	g/L
Organic part of sludge (VMLSS)	80	%
Excess sludge production	0,9	T SS/day
Return sludge flow	50	L/s
Hydraulic retention time	6 – 8	hours
Sludge retention time	8 - 12	days

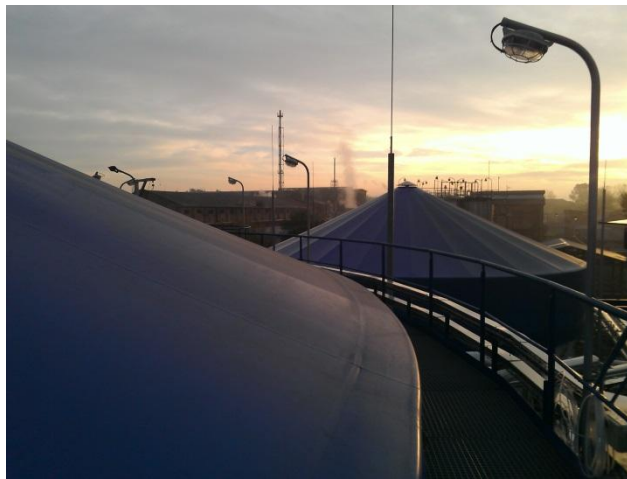
- Concentration of sludge is slightly lower then in classical activated sludge system.
- The organic part of the sludge is larger due to absence of suspended solids in the influent.

Wastewater quality

mg/L	N-NO ₃ ⁻	N-NH ₄ ⁺	COD	BOD	TSS	pH
Influent	240	0.4	100	25	20	1.5
Effluent	10	0.2	50	10	30	6 - 8

+ Removal of nitrates and adjustment of pH

— High operation costs



Operational problems

1) Severe inhibition of denitrification process

- Loss of ability to reduce nitrates
- Stopping the wastewater flow into WWTP
- Inhibitions lasted 8 - 48 hours

2) Poor sedimentation properties of sludge

- Problems with separation of the sludge in the settling tank
- Restriction of wastewater volume

Inhibition of denitrification

Nitrous gases above the surface of the denitrification reactor.

Possible causation: Nitric oxide

- Denitrification intermediate
- Free radical
- Toxic to bacteria

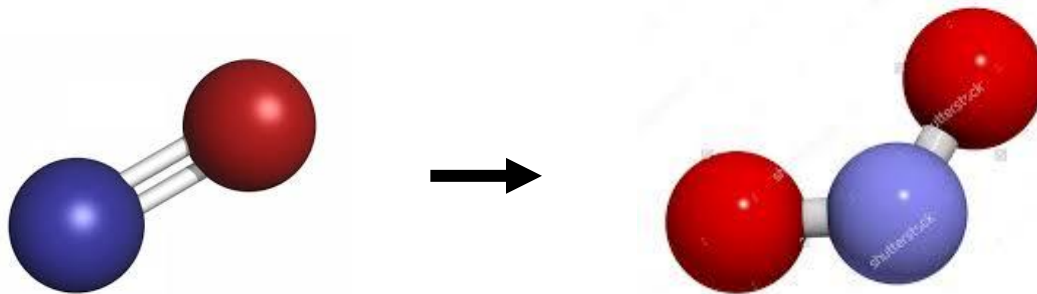
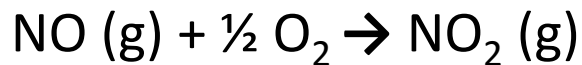
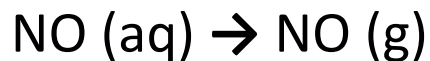


Theory of formation of nitric oxide

High nitrates loading, low pH \rightarrow accumulation of NO



After reaching solubility limit

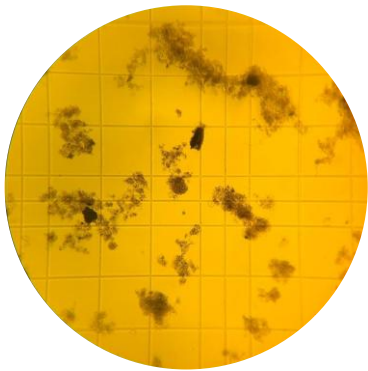


Poor sedimentation properties of sludge

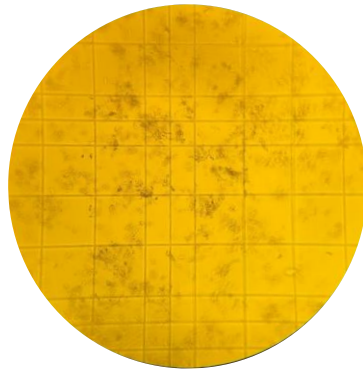
Zoogloal bulking = excessive amount of extracellular polymers. Polymers retain large amount of water and prevent the sludge flocs approaching to each other closely.

- slow sedimentation velocity
- poor dewatering

Normal activated and zoogloal sludge



Normal sludge



Zoogloal sludge



After 30 minutes



After 2 hours

Solution attempts

- Dosing of weighting material (milled limestone)
- Dosing of coagulant (Ferric Sulphate) and flocculant
- Partial change of substrate (Brenntaplus VP1)
- Dosing of micronutrients (Vithane)
- Decrease of sludge concentration in reactor

poor sedimentation vs. inhibition



Thank you for your attention



Královéhradecká
provozní